



1 Article

2 Predicting the Features of Methane Adsorption in 3 Large Pore Metal-Organic Frameworks for Energy 4 Storage

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11 **Abstract** : Currently metal-organic frameworks (MOFs) are receiving significant attention as part
12 of an international push to use their special properties in an extensive variety of energy
13 applications. In particular, MOFs have exceptional potential for gas storage especially for methane
14 and hydrogen for automobiles. However, using theoretical approaches to investigate this
15 important problem presents various difficulties. Here we present the outcomes of a basic
16 theoretical investigation of methane adsorption in large pore MOFs with the aim of capturing the
17 unique features of this phenomenon. We have developed a pseudo one-dimensional statistical
18 mechanical theory of adsorption of gas in a MOF with both narrow and large pores which is solved
19 exactly using a transfer matrix technique in the Osmotic Ensemble (OE). The theory effectively
20 describes the distinctive features of adsorption of gas isotherms in MOFs. The characteristic forms
21 of adsorption isotherms in MOFs reflect changes in structure caused by adsorption of gas and
22 compressive stress. Of extraordinary importance for gas storage for energy applications we find
23 two regimes of Negative gas adsorption (NGA) where gas pressure causes the MOF to transform
24 from the large pore to the narrow pore structure. These transformations can be induced by
25 mechanical compression and conceivably used in an engine to discharge adsorbed gas from the
26 MOF. The elements which govern NGA in MOFs with large pores are identified. Our study may
27 help guide the difficult program of work of computer simulation studies of gas storage in MOFs
28 with large pores.

29 **Keywords**: metal-organic framework; negative gas adsorption (NGA); osmotic ensemble (OE);
30 mechanical pressure; methane storage

32 1. Introduction

33 In the next few years, a revolution is expected to occur in energy storage that will modify the
34 way energy is used and the impact it creates on climate change [1,2]. The demand for energy storage
35 is rising rapidly as it is a key factor in the development of clean renewable energy technologies. New
36 cleaner electric vehicle technologies are replacing old dirty combustion engines. Yet, challenging
37 problems remain. The bridge between transportation using dirty combustion fossil fuel engines and
38 more versatile and cleaner newer designs is the focus of intense research endeavours but the main
39 problem remains the distance which electric automobiles can cover by battery power alone.

40 Storage of energy carriers (H₂, CH₄) in absorbent materials is a very promising innovative
41 energy solution [3,4] enhancing the driving range of hybrid electric automobiles. Metal-organic

1 frameworks (MOFs) are such absorbent materials which have become the focus of an international
2 endeavour to utilize their unique properties in an extensive range of energy applications [5,6].[7-9].
3 In particular, large pore MOFs are likely to be the best candidates for gas storage for energy
4 applications. Yet new and unexplored features and properties of these MOFs appear with increasing
5 pore-size. To be quite clear, these novel features appear when the change in volume in the narrow to
6 large pore transformation is such that the free energy contributions from the volume change become
7 dominant. The numerical values involved depends upon the pressure regime under consideration.
8 As is shown in detail below with pore sizes and volumes explicitly given, low pressure features
9 require large pore volume changes and vice versa.

10 MOFs are hybrid organic-inorganic nanoporous materials with remarkable adsorption
11 properties in which organic units link metal framework centres which afford structural flexibility
12 allowing transformations to occur between different pore systems. They make up a large class of soft
13 absorbent materials, designated by Kitagawa and co-workers [10] as “absorbent crystals that
14 possess both a highly ordered network and structural transformability”. MOFs have high potential
15 for use in adsorptive separation processes [11–12][13-19]. In MOFs metal framework centres and
16 organic units link thereby allowing structural transformations to occur upon adsorption of gas
17 [20-25] via rearrangement of the flexible linkers. Furthermore, temperature and pressure can also
18 cause structural transformations to occur [24, 26]. Coudert and co-workers [27] identify two
19 successive transformations, from a large pore (LP) to a narrow pore (NP) state and back again to the
20 LP state which they classify as guest induced structural transformations termed breathing and
21 opening of gates. These depend on applied conditions such as temperature and pressure, [23-26] as
22 well as adsorption [20-25] of gas molecules. Here we will show how pressure in particular can
23 transform structures with large pores with important implications for gas storage for automobiles.

24 Modelling these transformations [20-25] in MOFs is challenging and has attracted wide
25 attention. During the past few years [28-30] we have developed several solvable pseudo
26 one-dimensional statistical mechanical lattice theories of adsorption of gas on MOFs. Previously, we
27 considered [29] a pseudo-one dimensional statistical mechanical theory of adsorption in a
28 metal-organic framework (MOF) with both narrow and large pores which is solved exactly by a
29 transfer matrix method in the Osmotic Ensemble (OE). More recently [30] we considered a theory
30 treated in the OE to describe pure component and mixture adsorption in MOFs in structures which
31 can undergo pore transformation from narrow to large pores. The theory successfully describes the
32 form of adsorption of gas isotherms in MOFs which reflect structural transformations induced by
33 adsorption.

34 Even when somewhat physically unrealistic, solvable statistical mechanical models have made
35 a very significant contribution to developing the theory of condensed phases [31,32]. The model
36 which we discuss below is not a chemically realistic description of a particular MOF but is a
37 mathematically tractable theory of this material which displays all the expected characteristics of
38 adsorption of gas in a MOF with large pores and allowing identification of the important features of
39 this fundamentally and practically important problem. This work suggests the way forward for an
40 extensive experimental and theoretical program using Monte-Carlo techniques to study the
41 predictions made in this work.

42 Remarkably, in addition to opening of gates and breathing in MOFs [27], which is the result of
43 a transformation from a large pore (LP) to a narrow pore (NP) state, Krause et al. [33] recently
44 observed NGA in the large-pore MOF DUT-49 which has a pore-system comprising an assembly of
45 three pore-subsystems- cuboctahedral, tetrahedral and octahedral pores. Synchrotron powder X-ray
46 diffraction studies during methane adsorption at 111 K have revealed a structural “twisting”
47 transformation [34] of the large-pore structure DUT-49op at the pressure coinciding with the
48 negative adsorption step of the isotherm. While the cuboctahedral pores size does not change, the
49 size of the tetrahedral pores and especially the size of the octahedral pores decreases considerably.
50 This phenomenon observed by Coudert and collaborators [33] seems to play a central role in
51 large-pore MOFs for energy storage.

1 Usually, the adsorbed amount increases with gas pressure as the chemical potential of the
2 adsorbed component in the gas phase increases. However, methane adsorption isotherms at low
3 temperatures in DUT-49, a highly absorbent MOF, show a sudden decrease in adsorbed amount
4 with pressure at less than half of the full adsorption capacity of the adsorbent DUT-49 [33]. This
5 phenomenon was successfully simulated using grand canonical Monte-Carlo methods [34] and
6 appears rare amongst small pore MOFs. At low pressures, methane is adsorbed in the open pore
7 system of DUT-49 that has high adsorption capacity. After a certain amount has been adsorbed, an
8 adsorption induced transformation takes place of the open pore system to a much lower capacity
9 closed pore system. As the capacity of the closed pore system is lower than the adsorbed amount at
10 the transformation instance, the excess amount is removed from the MOF structure, manifested as
11 NGA which may be important technologically [35-39]. Most importantly, as we will discuss in
12 detail below, we find two regions of NGA in MOFs with large pores. Our theoretical study suggests
13 that NGA may actually be quite common in large pore MOFs and be a significant factor in the design
14 of gas storage in MOFs for energy applications.

15 In this paper we extend this work and present the results of a fundamental theoretical study of
16 small molecule adsorption in a generic large pore MOF with the purpose of identifying features
17 important in gas storage. Quite unexpected features occur which may have a very significant impact
18 on the use of MOFs in gas storage. Thus we extend our statistical mechanical theory to describe
19 adsorption of single components in a generic large pore MOF as a theory for a gas storage material.
20 Of great interest for gas storage we find two regions of NGA where gas pressure causes collapse of
21 the structure. These transformations can be driven by applied compressive stress and possibly
22 utilised in an engine to release adsorbed gas from the MOF. The factors which govern this NGA are
23 identified. We do not consider specific MOF structural details but focus on developing a statistical
24 mechanical theory which mimics the essential features of NGA and make predictions about the
25 adsorption behaviors of large pore MOFs.
26

27 **2. Pseudo-one Dimensional Model of Large-Pore Metal-Organic Frameworks.**

28 Some time ago we proposed an exactly solvable transfer matrix treatment of a statistical
29 mechanical lattice theory of a MOF which allows mixture and single component adsorption
30 isotherms and the compression of these soft materials to be theoretically described [30³⁰]. There is a
31 broadly held view [27] that the OE is the most appropriate theoretical formalism to model
32 adsorption in soft porous materials. The OE was developed initially by Brennan and Madden [40]
33 and Panagiotopoulos [41]. The theoretical approach taken here is an extension of our previous
34 development of an exactly solvable statistical mechanical lattice theory of a MOF in the OE using a
35 transfer matrix method which considers the treatments of the solid and gas components in an even
36 handed way [28-30].

37 Coudert and co-workers [42,43] in particular developed the OE for molecular simulation of
38 adsorption in MOFs. In his seminal text Hill [44] has discussed a number of 'Generalized
39 Ensembles' and the OE belongs in this class. For the OE the independent thermodynamic variables
40 are temperature, T , the number unit cells N in the MOF, the compressive stress σ and the chemical

41 potentials μ_a of the gas molecules a . The compressive stress σ and the chemical potential μ_a are
42 assumed to be independent variables.

43 Here we develop this transfer matrix treatment of a pseudo-one dimensional statistical
44 mechanical OE theory of pressure and adsorption induced structural transformations in MOFs with
45 large pores and in this way predict that NGA is common in such solids. The evaluation of the
46 Osmotic Potential requires the solution of a matrix eigenvalue problem which may be treated
47 computationally or exactly in some cases. It is found that for weak unit-cell interactions we can
48 calculate all the eigenvalues of the OE transfer matrix analytically.

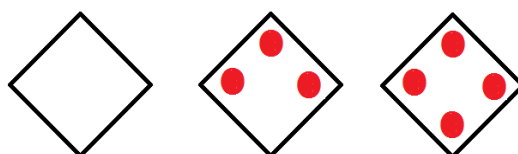
1 We consider a chain of N groups of unit cells each, which may be in either a narrow pore (NP)
 2 or large pore (LP) state with volumes v_{NP} and v_{LP} , the NP and LP volumes which are variable
 3 but typically 5000\AA^3 , 10000\AA^3 respectively yielding a 40% volume difference between these 2 states.
 4 The chain runs along the x -direction and is compressed by mechanical compressive stress σ (loosely
 5 termed pressure) parallel with this axis as shown in Figure 1. If no external stress is applied, the
 6 mechanical stress is equal to the gas pressure P but otherwise σ and P are independent variables. The
 7 stress term σ includes the gas pressure P and any applied compressive stress. The NP can be filled by
 8 up to a monolayer of gas molecules as depicted in Fig.1A. However, the LP can have adsorbed
 9 multilayers as shown in Fig. 1B. Fig. 1C shows an example of a typical configuration of a group of
 10 species considered in the infinite pseudo-one dimensional chain. The structure is subjected to a
 11 mechanical compressive stress σ (pressure) directed along the x -axis. The NP on the far left Fig.1C is
 12 vacant while the next small pore contains 3 methane molecules in the first adsorbed layer (red); the
 13 next LP to the right contains 8 molecules in the first layer and 4 (blue) in the second layer etc.
 14 Molecules are treated as spheres. All energetically allowed configurations and cell occupations are
 15 taken into consideration. The numbers of molecules in the NP and LP are variables in the theory. In
 16 all figures 1A, 1B, 1C molecules in the first monolayer are shown in red and blue in the second layer.
 17 In reality much larger NPs and LPs are considered but these are difficult to display.

18 The above description is clearly limited but it is a theory which straightforwardly yields
 19 predictions of the compressive and adsorption properties of MOFs which are difficult and expensive
 20 to obtain otherwise. This approach is not a substitute for more demanding computer simulations of
 21 three dimensional MOFs nor do we expect the empirical parameters found for our pseudo-one
 22 dimensional theory to realistically describe a real MOF. Compared with simulation based
 23 approaches our aims and objectives differ somewhat. Accurately treated statistical mechanical
 24 models may easily give original predictions of novel behavior in MOFs. Hence, our purpose is to
 25 construct a methodology which enables the broad features of NGA isotherms to be calculated easily
 26 and cheaply and which may give up new insights into these materials.

27

(A)

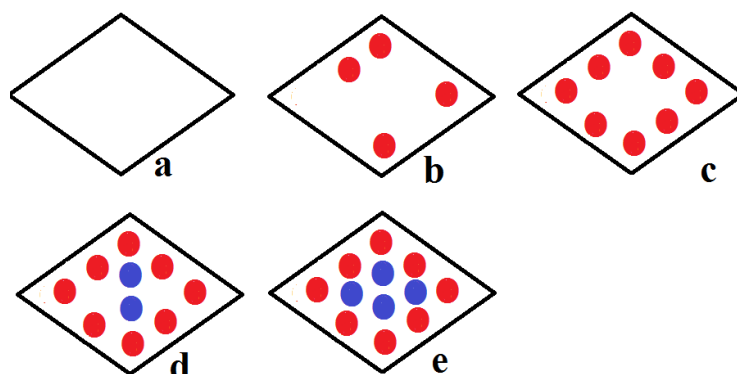
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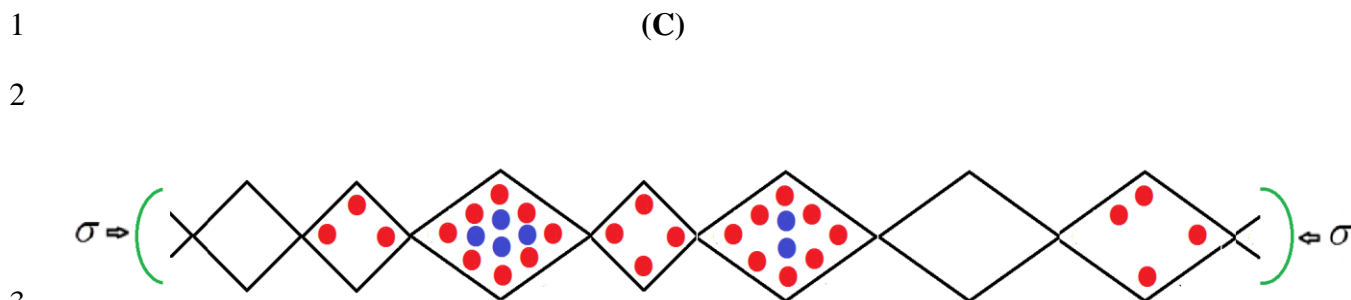
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(B)



31



4 **Fig. 1.** (A) Vacant, partially filled and full Narrow pore. (B) Large pore (a) vacant (b) partially filled
 5 first layer (c) filled first layer (d) filled first layer and partially filled second layer (e) fully filled large
 6 pore. (C) An example of a typical arrangement of a cluster of molecules considered in the pseudo-one
 7 dimensional chain.

8 All energetically allowed occupations and configurations are permitted in the theory. The chain
 9 is compressed by a stress σ (pressure) directed along the x -axis. The small pore (NP) on the
 10 extreme left is vacant while the next small pore contains 3 methane molecules in the first adsorbed
 11 layer (red); the next LP to the right contains 8 molecules in the first layer and 4 (blue) in the second
 12 layer etc. Molecules are treated as spheres. The numbers of molecules in the NP and LP are
 13 variables in the theory.

14 In all figures molecules in the first monolayer are shown in red and blue in the second layer. In
 15 reality much larger NPs and LPs with many molecules are considered. However, these are difficult
 16 to display, but they are defined in the captions of figures below.

17 The adsorbed species occupying the cells are in equilibrium with those in an ideal gas phase at
 18 pressure P and temperature T with chemical potential $\mu = \mu^0 + kT \ln(P)$ where the standard

19 chemical potential μ^0 is given by $\mu^0 = -kT \ln \left[\left(\frac{2\pi m kT}{h^2} \right)^{3/2} kT \right]$ and where non-ideality

20 behaviour can be introduced substituting pressure by fugacity, see Hill [45]. m is the molecular
 21 mass, k is Boltzmann's constant and h is Planck's constant.

22 For species adsorbed in the one-dimensional chain of N cells, the Osmotic Partition function
 23 $\Phi(\sigma, T, \mu)$ is:

$$\Phi(\sigma, T, \mu) = \sum_V \sum_n \exp\left(-\frac{\sigma V}{kT}\right) Q(n, V, T) \exp\left(\frac{\mu n}{kT}\right) \quad (1)$$

24 $Q(n, V, T)$ is the Canonical partition function for volume V . The Osmotic Potential Ω is
 25 $\Omega = -kT \ln \Phi$ calculated in this application from the logarithm of the maximum term in the
 26 Osmotic partition function. Here we evaluate this accurately by a transfer matrix method and hence
 27 compute adsorption isotherms.

28 Hence, the logarithm of the maximum term in the series eqn. (1) is:

$$\ln \Phi = -\frac{\sigma V^*}{kT} + \ln Q(n^*, V^*, T) + \frac{\mu n^*}{kT} \quad (2)$$

29 The starred (*) symbol indicates optimum values n^*, V^* which are required to be solutions to
 30 the extremum equations

$$\left(\frac{\partial \ln \Phi}{\partial V}\right) = \frac{-\sigma}{kT} + \left(\frac{\partial \ln Q}{\partial V}\right) = 0$$

$$\left(\frac{\partial \ln \Phi}{\partial n}\right) = \left(\frac{\partial \ln Q}{\partial n}\right) + \frac{\mu}{kT} = 0 \quad (3)$$

1 These expressions are identical to those for pressure and chemical potential in a canonical
2 ensemble demonstrating that use of Maximum term methodology has caused the OE to degenerate
3 into a Canonical ensemble [45]. Differentiation of equation (2) yields

$$-d(kT \ln \Phi) = V^* d\sigma - SdT - n^* d\mu \quad (4)$$

5 giving for the optimum values n^*, V^* :

$$V^* = -kT \left(\frac{\partial \ln \Phi}{\partial \sigma}\right) \quad (5)$$

$$n^* = kT \left(\frac{\partial \ln \Phi}{\partial \mu}\right)$$

6 $\ln \Phi$ is obtained using the transfer matrix method described in the next section.

7 3. Transfer Matrix Method for Calculation of Adsorption Isotherms for Large-Pore 8 Metal-Organic Frameworks.

9 We have earlier made a review of matrix methods for the calculation of adsorption isotherms
10 for one-dimensional lattice fluids [46]. A recent application of this approach to MOFs has been given
11 by Simon et al. [47].

12 The Osmotic partition function equation (1) can be expressed as [29]:

$$\Phi = \sum_{\alpha=1}^j \sum_{\beta=1}^j \sum_{\gamma=1}^j \dots \sum_{\omega=1}^j A_{\alpha\beta} A_{\beta\gamma} A_{\gamma\delta} \dots A_{\omega\alpha} \quad (6)$$

13 By wrapping the chain on to a ring cyclic boundary conditions will be imposed. In the matrix
14 formalism we specify the terms $A_{\alpha\beta}$ in (6) as the multiple of the internal partition functions f_α for
15 cluster α and f_β for cluster β and an intercluster interaction expression given by:

$$A_{\alpha\beta} = (f_\alpha f_\beta)^{1/2} e^{-\varepsilon_{\alpha\beta}/kT} \quad (7)$$

16 The variables α, β span all clusters 1 to j and where $\varepsilon_{\alpha\beta}$ is the interaction energy between these.

17 We have noticed that the important features of the MOF adsorption isotherms can be obtained
18 by considering two extreme cases by choosing particular values of $\varepsilon_{\alpha\beta}$. This parameter is set to zero
19 or infinitely repulsive and this choice defines theories A and B below.

20 Using standard matrix algebra we have $D_{ij} = \sum_k B_{ik} C_{kj}$ for the inner matrix product of a
21 pair of conformable matrices **B** and **C**. Hence the Osmotic Partition function (6) is given as

$$\Phi(\sigma, T, \mu_a, \mu_b) = \sum_{\alpha=1}^j (\mathbf{A}^N)_{\alpha\alpha} = \text{Tr}(\mathbf{A}^N) = \sum_{i=1}^j (\lambda_i)^N \quad (8)$$

22 The transfer matrix **A** has elements

$$A_{ij} = (f_i f_j)^{1/2} e^{-\varepsilon_{ij}/kT} \quad (9)$$

24

1 and has eigenvalues $\lambda_1, \lambda_2, \lambda_3, \dots, \lambda_j$. Only the largest eigenvalue λ_{\max} of \mathbf{A} is required in
 2 matrix evaluations of partition functions since for large N equation (6) reduces to

$$\Phi(\sigma, T, \mu) = (\lambda_{\max})^N \quad (10)$$

3 Δ is the energy cost to transform the more stable LP conformer to the NP conformation.
 4 We will assume in this minimum theory that the narrow pore only has a single layer.
 5 For n_1 molecules adsorbed in the first monolayer of the LP we assume that a cluster of
 6 molecules and vacancies occupy $N_{\max LP}$ sites. With n_1 molecules there are $(N_{\max LP} - n_1)$
 7 holes or vacancies giving rise to a configurational degeneracy (the first factor on the right
 8 hand side in equation 11).

9 For a cluster containing n molecules the number of pair interactions is estimated as $(n^2 - n) / 2$
 10 . If the mean interaction energy is J , the total interaction energy is $J(n^2 - n) / 2$.

11 Thus the cluster partition function f_{LP, n_1} for the first monolayer of molecules in the LP
 12 containing n_1 molecules is

$$f_{LP, n_1} = \frac{N_{\max LP_1}!}{(N_{\max LP_1} - n_1)! n_1!} \exp\left(\frac{-\sigma U_{LP}}{kT}\right) \left(\exp\left(\frac{-u_{LP_1} + \mu}{kT}\right)\right)^{n_1} \exp\left(\frac{-J(n_1^2 - n_1) / 2}{kT}\right) \quad (11)$$

13 Where u_{LP_1} is the adsorption energy of a molecule in the first monolayer in the LP.
 14 Using similar arguments, a NP cell containing n_1 species has a contribution to the Osmotic
 15 partition function

$$f_{NP, n_1} = \frac{N_{\max NP_1}!}{(N_{\max NP_1} - n_1)! n_1!} \exp\left(\frac{-\sigma U_{NP} - \Delta}{kT}\right) \left(\exp\left(\frac{-u_{NP_1} + \mu}{kT}\right)\right)^{n_1} \exp\left(\frac{-J(n_1^2 - n_1) / 2}{kT}\right) \quad (12)$$

18 After the first layer in the LP is filled multilayer adsorption can occur. The large pore has
 19 molecules adsorbed in other layers which are not tightly bound. The partition function for these
 20 multilayer species containing Nm molecules is given by

$$f_{LP, N_m} = \frac{N_{outer}!}{(N_{outer} - N_m)! N_m!} \exp\left(\frac{-\sigma U_{LP}}{kT}\right) \left(\exp\left(\frac{-u_{outer} + \mu}{kT}\right)\right)^{N_m} \exp\left(\frac{-J(N_m^2 - N_m) / 2}{kT}\right) \\ \times \exp\left(\frac{-u_{LP} + \mu}{kT}\right)^{N_{\max LP}} \exp\left(\frac{-J(N_{\max LP}^2 - N_{\max LP}) / 2}{kT}\right) \quad (13)$$

23 N_{outer} is the number of sites in the outer layer, and where the energy of adsorption u_{outer} is
 24 scaled (by a factor 'scale' in the figure captions below) to give a reduction factor in the well-depth
 25 and also takes account phenomenologically of interlayer interactions.

26 4. Eigenvalues of the Transfer Matrix

1 To calculate adsorption isotherms the largest eigenvalue of the transfer matrix given in
 2 equation (9) is needed and usually this must be obtained by computational means. However, we
 3 have studied two particular relevant cases where it is possible to find all the eigenvalues of the
 4 Transfer Matrix algebraically by exploiting elements of the theory of symmetrical matrices. For the 2
 5 cases with the block structures shown in eqns (15),(16) below, it is demonstrated in ref [30] that the
 6 largest eigenvalue of the appropriate block is

$$\lambda_{\max} = \left(\sum_{i=1}^j f_i \right) \quad (14)$$

7 and all the other eigenvalues are zero.

8 The matrix A (defined by equation (9)) can be partitioned into two main blocks which describe
 9 LP and NP cell types and off-diagonal blocks which implement the coupling between these two
 10 types of conformations as indicated below

$$\begin{pmatrix} \mathbf{A}_{LP,LP} & \mathbf{A}_{LP,NP} \\ \mathbf{A}_{NP,LP} & \mathbf{A}_{NP,NP} \end{pmatrix} \quad (15)$$

11 The coupling (or otherwise) of the main diagonal blocks by the off-diagonal blocks gives to two
 12 types of theories - A and B.

13 Coudert and co-workers [48] assume that LP and NP phases do not exist simultaneously in a
 14 perfect crystal. In such a situation off-diagonal couplings are zero giving the matrix

$$\begin{pmatrix} \mathbf{A}_{LP,LP} & \mathbf{0} \\ \mathbf{0} & \mathbf{A}_{NP,NP} \end{pmatrix} \quad (16)$$

15 The main diagonal blocks in this matrix decouple and this permits calculations to be made for
 16 ordered crystals, which we call theory A in reference [30], and here 'sharp transition theory'.

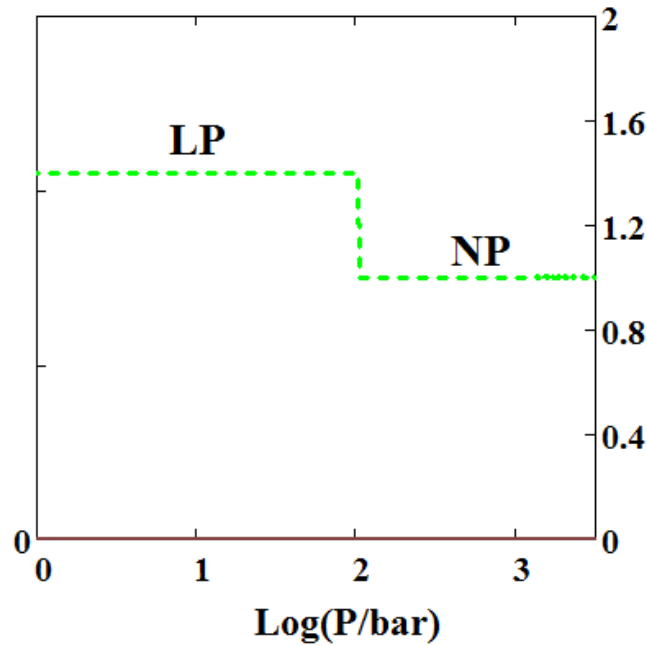
17 Introduction of this off-diagonal coupling permits consideration of short range ordered phase
 18 mixtures which we call theory B in reference [30], and here 'gradual transformation theory'.

19 Below we present some results for both theories as appropriate to the level of disorder in the
 20 MOF sample.

21 5. Effect of Compressive stress on a MOF

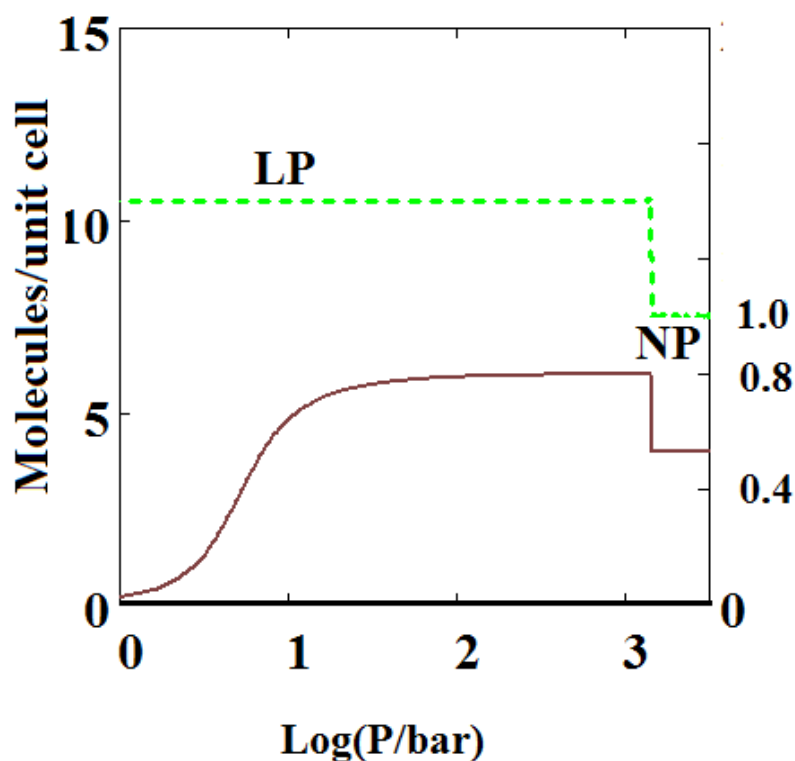
22 Mercury intrusion experiments have been undertaken by Beurroies et al. [49] and Yot et al. [50]
 23 in which a powdered sample of the MOF MIL-53 is brought under isotropic mechanical stress
 24 causing the powder to increase in density. Such a mechanical stress corresponds crudely to the
 25 compressive stress (loosely termed a mechanical pressure σ in our theory). Later Neimark et al.
 26 [22-24] observed a LP to NP transformation at a pressure of 550 ± 150 bar. We have modelled this
 27 compression induced density change by calculating the solid volume as a function of the mechanical
 28 compression of a theory of MIL-53 parameterised as in ref [30] to give good description of pure
 29 methane adsorption isotherms. Fig. 2A below shows compression of the structure, which is in
 30 reasonable agreement with the results in the above studies. The same theory was used and Fig.2B
 31 shows an adsorption isotherm calculated for pure methane for MIL-53. The adsorption isotherm
 32 shows NGA at about 1000 bar which is about the same mechanical pressure as the intrusion
 33 experiments undertaken by Beurroies et al. [49] while Neimark et al. [24] showed collapse of the

1 MIL-53 structure when brought under isotropic mechanical stress causing the powder to increase in
 2 density. The pressure at which NGA occurs increases in the model with increasing heat of
 3 adsorption indicating that it is harder to compress the MOF containing more strongly bound
 4 molecules. As the temperature is lowered to below 284 K our calculations also show that MIL-53
 5 breathes in pure methane where the NP plays a significant role [30]



6

7 **Fig.2 A.** Mechanical compression of MIL-53 at 300K for using the parameters given in ref [30]. At
 8 higher pressures there is a mechanical compression of the MOF to the NP state. The axis on the right
 9 measures the volume in units of the NP volume.



10

1 **Fig.2 B.** Adsorption isotherms of pure methane calculated using sharp transformation approach at
2 300 K using the pure methane parameters given in ref [30] for MIL-53. At higher pressures there is
3 NGA caused by the compression of the MOF to the NP state. The axis on the right measures the solid
4 volume in units of the NP volume.

6 6. Isotherms Showing Negative Adsorption of Gas at Low Pressure

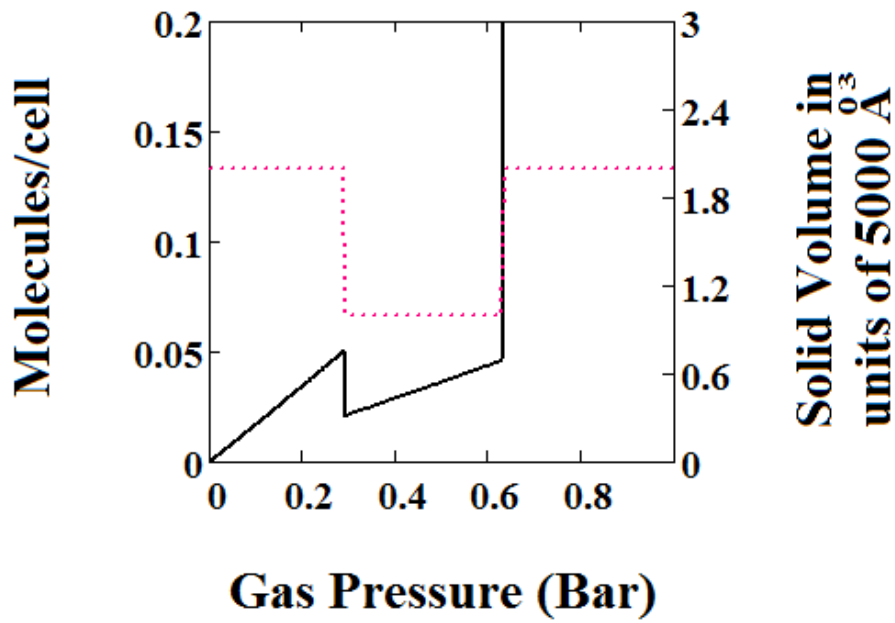
7 Adsorption isotherms have been calculated and presented in Figs.3-5 using parameters shown
8 below the figures. The energies of adsorption of the pure components and maximum occupations for
9 the large (2 types of site) and narrow pores are parameterized and given in the figure captions. Δ is
10 the energy difference between the LP and NP states and is the energy required to convert from the
11 more stable LP to NP.

12 Calculation of MOF volumes and adsorption isotherms was performed straightforwardly
13 using the above methodology and the Mathcad 15 software package [51]. Finite difference
14 calculation of derivatives was performed.

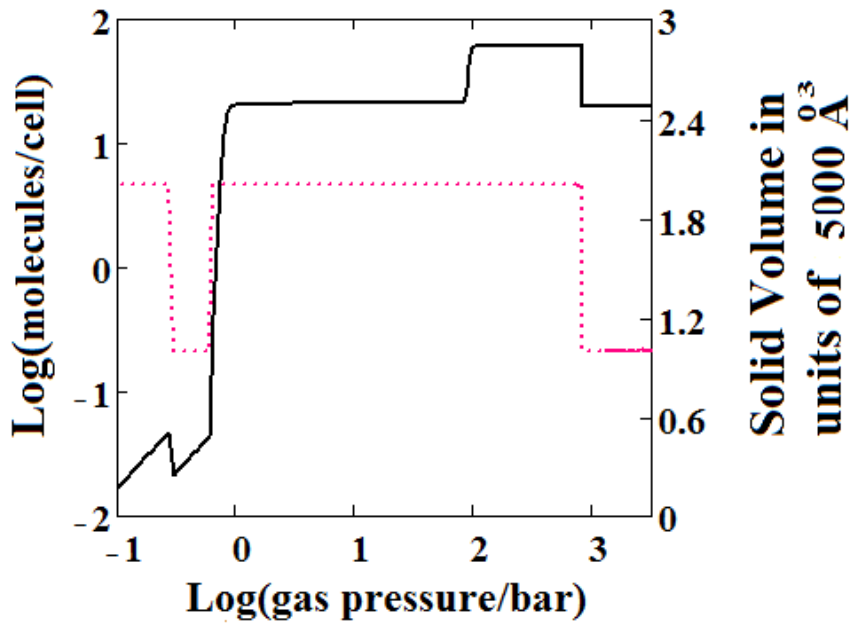
15 The methane adsorption isotherm in Fig. 3A shows a negative adsorption at around 0.3 bar
16 which is the result of the LP to NP transformation at the same pressure. The vacant MOF is in the
17 LP state. If we consider each pore system on their own, LP or NP, having their individual isotherms
18 [48], then the resulting isotherm can be considered to be constructed from the segments of the
19 individual isotherms of the stable pore system. Usually in the low pressure region, the LP isotherm
20 lies below the NP isotherm [48]. As a result, when the LP to NP transformation occurs, the
21 adsorption isotherm shows a positive step, as normal. Under some conditions, such as those in the
22 experimental work [33] and our calculations presented here, the LP- NP isotherms at low pressure
23 reverse. Under these conditions, the LP isotherm lies above the NP. Hence, the LP to NP
24 transformation causes a negative adsorption step.

25 Fig. 3B, which is a log-log plot of the same isotherm and extends to much higher pressures,
26 shows a second negative adsorption just below 1000 bar, when the NP system is transformed back
27 to the LP one. This adsorption step is negative because at those pressures, LP has higher adsorption
28 capacity than NP. Before this, at about 100 bar, the isotherm shows a positive adsorption step in
29 the LP state. Up to this step, the adsorption takes place in the first adsorption monolayer which is
30 saturated fast after the NP to LP transformation at 0.3 bar, while at around 100 bar the inner core of
31 the LP theory, second layer, fills rapidly. This behaviour arises for a wide range of theory
32 parameters as for example the ones in Fig. 4.

33 Similar behaviour is also shown by the gradual transformation theory [30], Fig. 5. Rather than
34 sharp adsorption steps, the MOF structure shows a gradual negative adsorption at the pressure
35 range 20-30 bar. In the gradual transformation theory the coexistence of LPs and NPs is permitted.
36 As the solid volume curve in Fig. 5 shows, at 1 bar a mixture of NPs and LPs coexist. With
37 increasing pressure, LPs are transformed to NPs. This transformation is complete at around 5 bar,
38 where both curves level, the adsorption isotherm as well as the solid volume to the LP volume
39 value. At around 20 bar, the reverse transformation of LPs to NPs starts taking place which causes a
40 gradual negative adsorption. In Fig.5 the first negative adsorption transformation shown in Fig.4 is
41 lost.



(A)



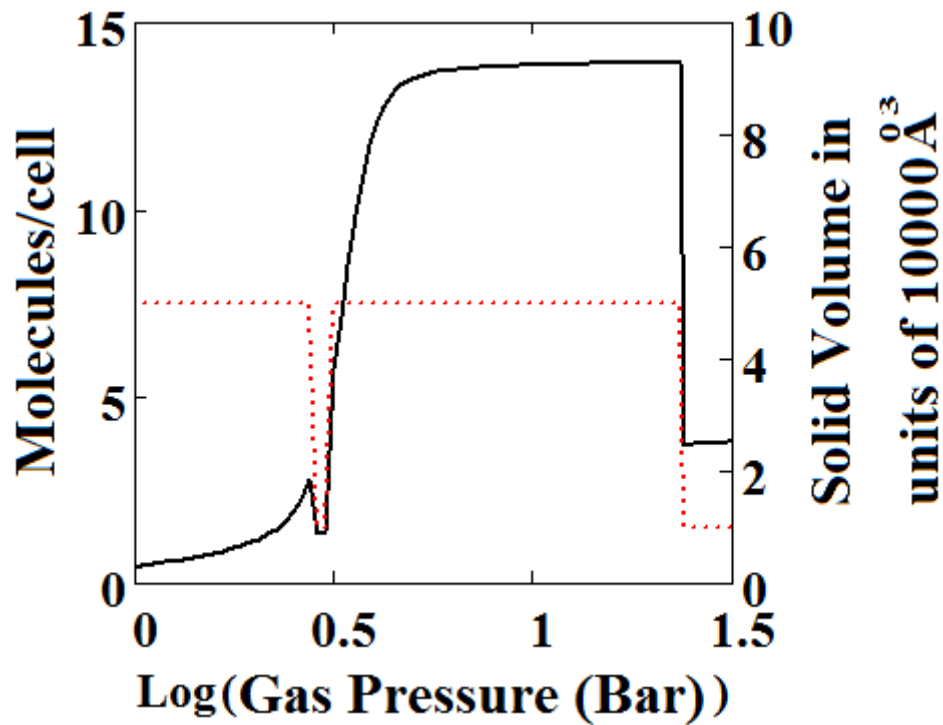
(B)

Fig. 3. (A) Methane adsorption in the theory MOF showing NGA. The dotted red curve on the secondary right axis indicates the NP/LP state of the MOF. The other parameters are $T=257 \text{ K}$, $u_{glp}=-14.8 \text{ kJ/mole}$, $u_{gnp}=-13.55 \text{ kJ/mole}$, $J=-1.08 \text{ kJ/mole}$, $X=5000 \text{ \AA}^3$, $Y=10000 \text{ \AA}^3$, $\Delta=0.025 \text{ kJ/mole}$, $N_m=40$, $scale=0$, $n_{maxlp}=21$, $n_{maxnp}=20$. (B) Same methane adsorption in the theory MOF on a Log-Log scale showing 2 regions of NGA.

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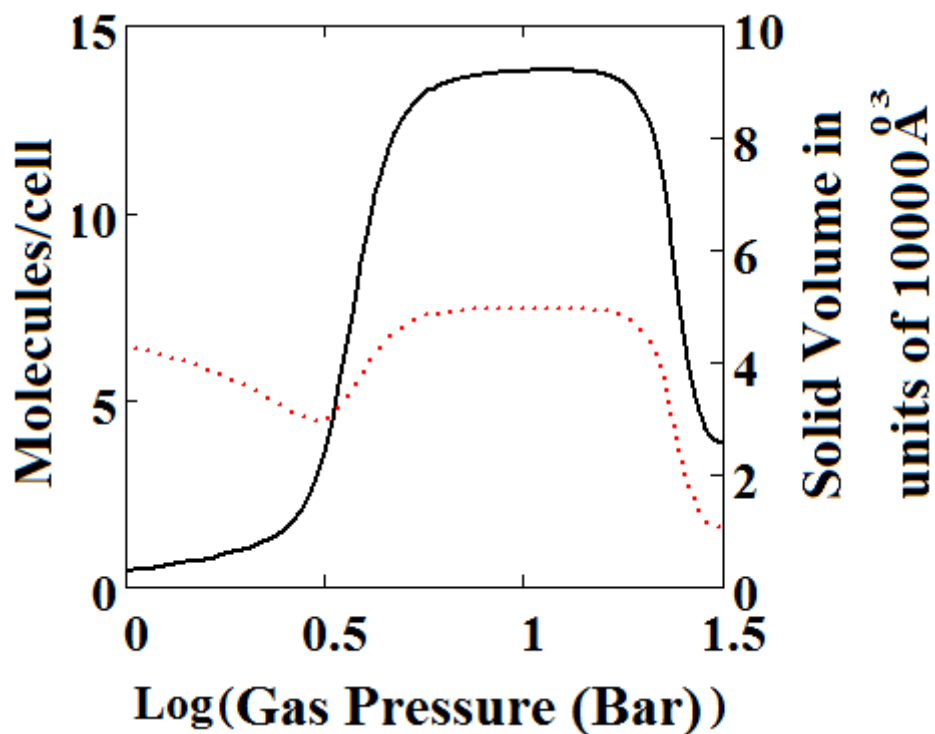
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Fig. 4. Methane adsorption in the theory MOF showing two regions of NGA. The dotted red curve on the secondary right axis indicates the NP/LP state of the MOF. The other parameters are $T=285\text{ K}$, $u_{glp}=-29.1\text{ kJ/mole}$, $u_{gnp}=-28.69\text{ kJ/mole}$, $J=-1.66\text{ kJ/mole}$, $\Delta=5.8\text{ kJ/mole}$, $X=10000\text{ \AA}^3$, $Y=50000\text{ \AA}^3$. At high gas pressure the MOF is compressed into the NP state. The behaviour shown at high pressure should be almost universal for MOFs. Numb=10, scale=0.85, nmaxlp=4, nmaxnpb=4 (sharp transformation theory). Compare with Fig. 8.



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Fig. 5. Plot of the behaviour of the methane adsorption in the theory MOF showing two regions of NGA transformation. The dotted red curve on the secondary right axis indicates the NP/LP state of the MOF. The other parameters are $T=285\text{ K}$, $u_{glp}=-29.1\text{ kJ/mole}$, $u_{gnp}=-28.69\text{ kJ/mole}$, $J=-1.66$

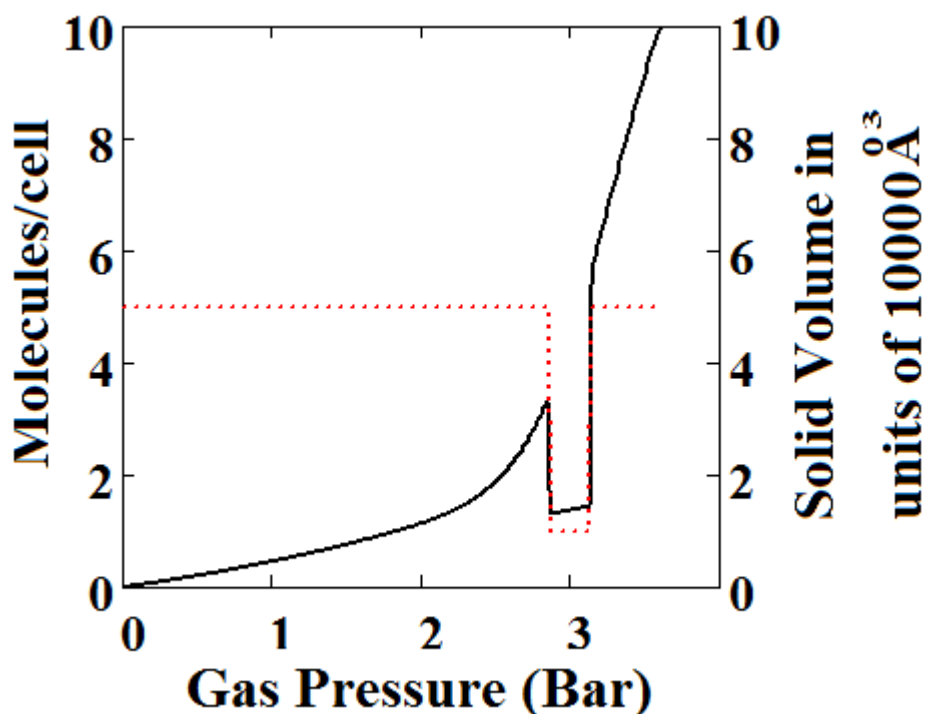
1 kJ/mole, $\Delta = 5.8$ kJ/mole, $X = 10000 \text{ \AA}^3$, $Y = 50000 \text{ \AA}^3$. At high gas pressure the MOF is compressed
 2 into the NP state. The behaviour shown at high pressure should be almost universal for MOFs.
 3 $N_m = 10$, $\text{scale} = 0.85$, $n_{\text{maxlp}} = 4$, $n_{\text{maxnpb}} = 4$ (gradual transformation theory). Compare with Fig.4.

4 7. Influence of Mechanical Pressure on Adsorption Isotherms

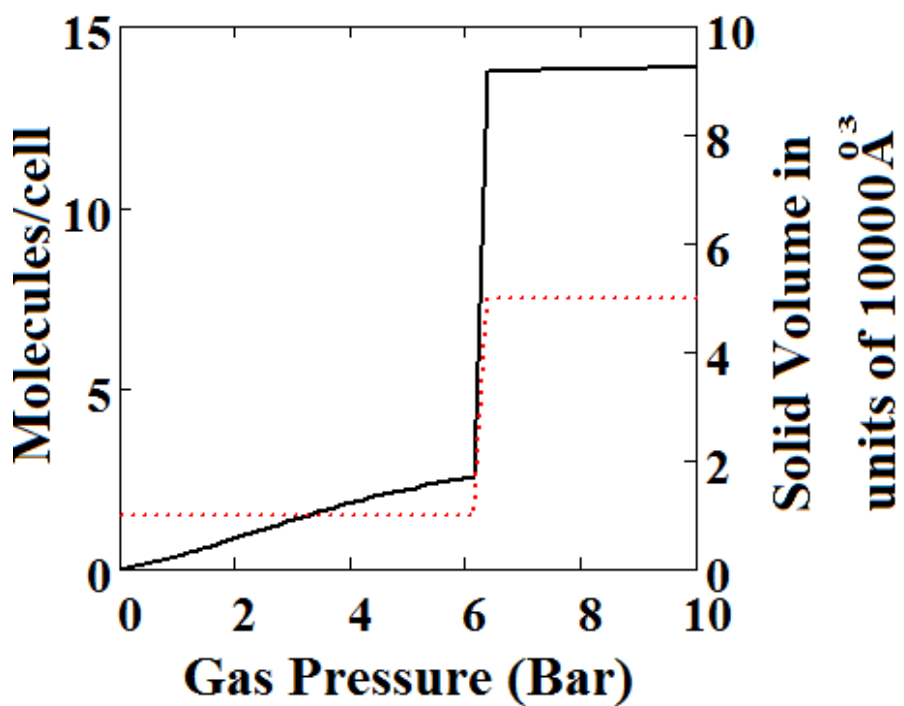
5 We have calculated using Theory A (sharp transformation approach) adsorption isotherms (Fig.
 6 6) when the MOF structure is subjected at various additional compressive stresses over a range of
 7 gas phase pressures as shown in Fig. 6. In Fig. 6A no additional compressive stress is applied, while
 8 in Figs. 6B and 6C additional mechanical pressures of 10 and 100 bar respectively are applied. It may
 9 be seen that the negative adsorption disappears in Figs. 6B and 6C with the application of additional
 10 compressive stress. Under 10 bar (Fig. 6B) additional compressive stress, at low gas pressures the
 11 MOF is in the NP state transforming to the LP at higher gas pressures, while at 100 bar (Fig. 6C) the
 12 transformation does not occur at all, the system remains in the NP state for the pressure range
 13 considered. The application of additional compressive stress squeezes the MOF structure into the
 14 NP state, such that in all cases the system remains in the NP state.

15 In Fig. 6D we show the effect of increasing mechanical pressure on the density of the MOF in
 16 the absence of gas pressure. It can be seen that the system is in the LP state at low compression and
 17 collapses to the NP state at about 2.5 bar. This pressure is close to the gas pressure shown in Fig. 6A
 18 at which the MOF shows NGA.

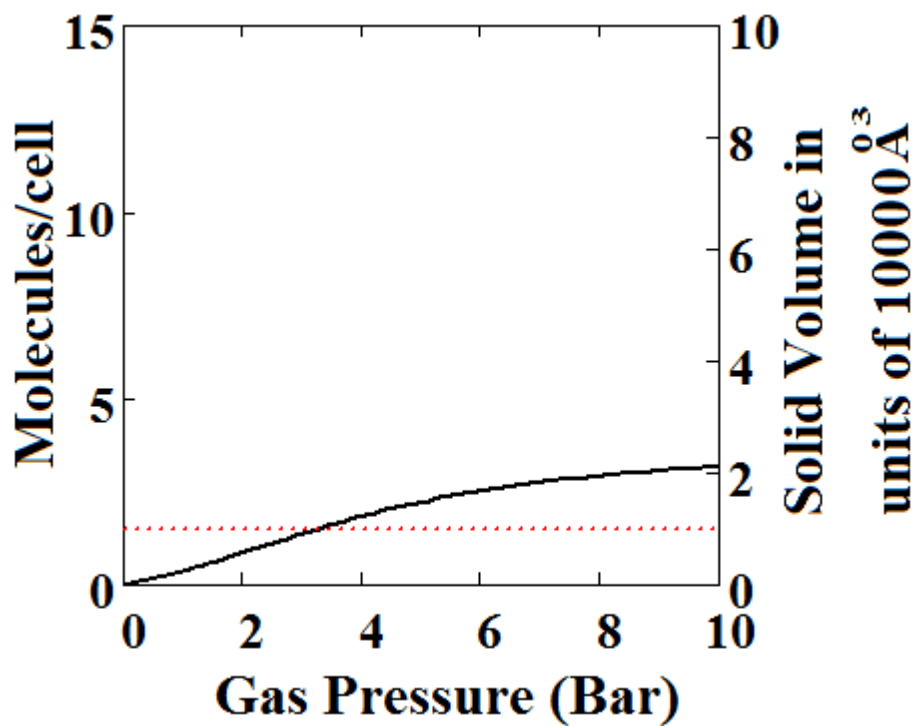
19 When adsorbents are used for gas storage, slow release of the gas is problematic. It seems
 20 possible that in an MOF with a slow desorption kinetics being used for gas storage, application of
 21 mechanical compression might speed up the release of gas.



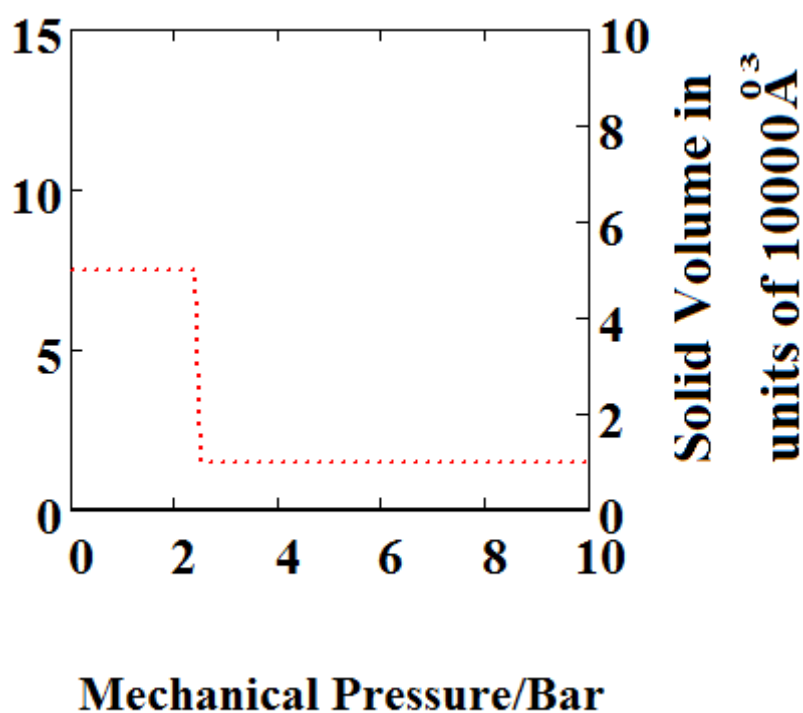
22 (A)



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2 (B)



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4 (C)



(D)

Fig. 6. Plot of the behaviour of the methane adsorption in the theory MOF under an additional applied mechanical pressure of (A) 0 Bar (B) 10 Bar (C) 100 Bar. In (B), (C) the NGA transformation shown in (A) has disappeared. The dotted red curve on the secondary right axis indicates the NP/LP state of the MOF. (D) Plot of the density behaviour of the MOF under an applied compressive stress. The dotted red curve on the secondary right axis indicates the NP/LP state of the MOF.

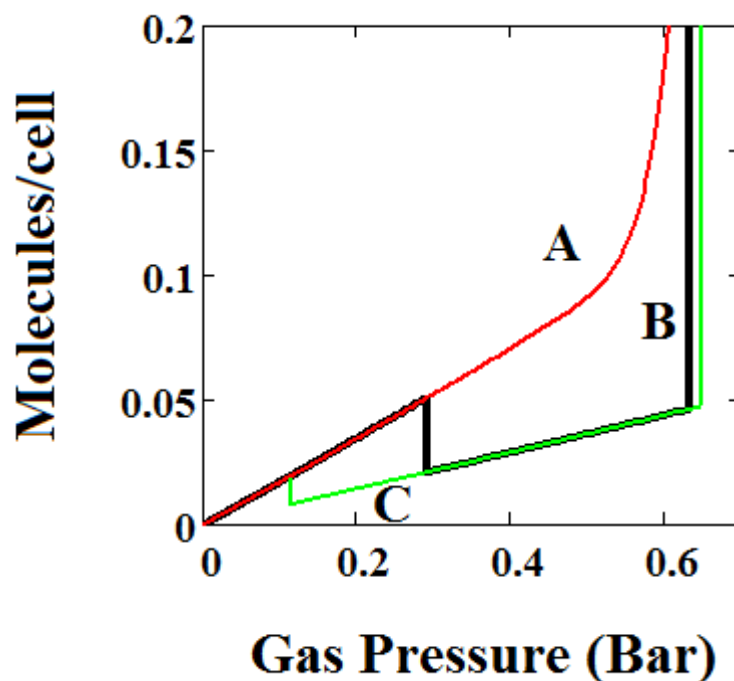
The other parameters are $T=285$ K, $u_{lp}=-29.1$ kJ/mole, $u_{np}=-28.69$ kJ/mole, $J=-1.66$ kJ/mole, $\Delta=5.8$ kJ/mole, $X=10000\text{\AA}^3$, $Y=50000\text{\AA}^3$, $N_m=10$, $scale=0.85$, $n_{maxlp}=4$, $n_{maxnp}=4$.

8. Effect of various parameters on NGA: Intermolecular interactions, heat of adsorption, pore transformation energy.

In Figs. 2-6 we have shown examples of NGA for a wide range of model parameters. Figs. 7, 8 and 9 show the effect of variation of the parameters representing pore transformation energy on the adsorption isotherms (Δ), intermolecular interactions (J) and differences in values of the LP and NP heats of adsorption.

The behaviours shown are consistent with the importance of these terms in the osmotic potential Ω given by $\Omega = -kT \ln \Phi$ where the system minimises this potential. Thus in Fig. 7 the system with the lowest value of Δ undergoes a negative adsorption transformation most readily while in Fig. 8, the system with the lowest value of J (intermolecular interactions in LP) undergoes a negative adsorption transformation most readily. Thus, low values of Δ shift the NGA transformation to lower pressures while high values cause the transformation to disappear, while high J values cause the NGA transformation to disappear.

In Fig. 9, isotherms are compared for 3 pairs of differences in values of the LP and NP heats of adsorption (A=-13.00 and -18.96, B=-16.6 and -13.55, C=-14.8 and -13.55, kJ/mole). Curve C shows an NGA transformation at low pressure on the left. For the NGA transformation to occur the LP, NP heats of adsorption should be close in magnitude.



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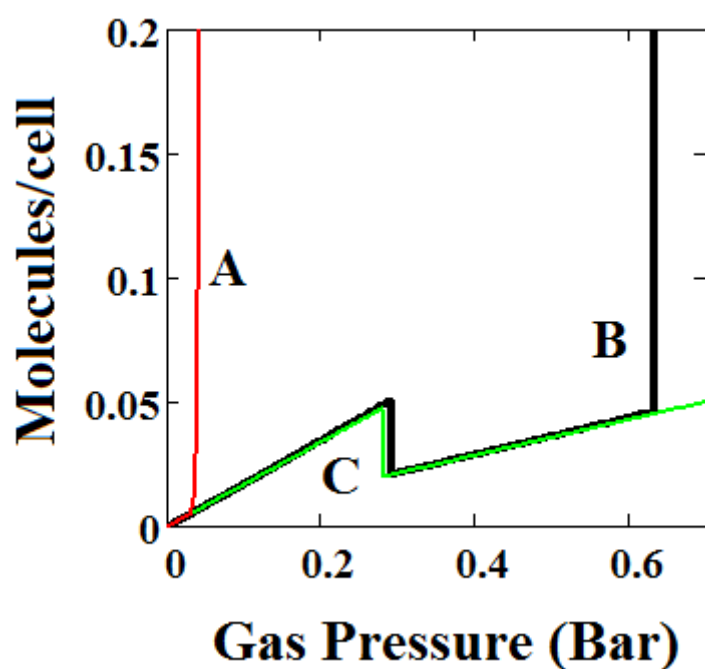
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Fig. 7. Plot of the behaviour of the methane adsorption in the theory MOF for 3 values of the parameter Δ ($A=0.05$, $B=0.025$, $C=0.01$ kJ/mole). Curves B, C show a NGA transformation. Low values of Δ shift the NGA transformation to lower pressures while high values cause the transformation to disappear. The other parameters are $T=257$ K, $u_{glp}=-14.8$ kJ/mole, $u_{gnp}=-13.55$ kJ/mole, $J=-1.08$ kJ/mole, $X=5000\text{\AA}^3$, $Y=10000\text{\AA}^3$, $N_m=40$, $scale=0$, $n_{maxlp}=21$, $n_{maxnpb}=20$.



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Fig. 8. Plot of the behaviour of the methane adsorption in the theory MOF for 3 values of the parameter J ($A=-2.29$, $B=-1.49$, $C=-0.573$ kJ/mole). Curves B, C show a NGA transformation. High J values cause the NGA transformation to disappear. The other parameters are $T=257$ K, $u_{glp}=-14.8$ kJ/mole, $u_{gnp}=-13.55$ kJ/mole, $\Delta=0.025$ kJ/mole, $X=5000\text{\AA}^3$, $Y=10000\text{\AA}^3$, $N_m=40$, $scale=0$, $n_{maxlp}=21$, $n_{maxnpb}=20$.

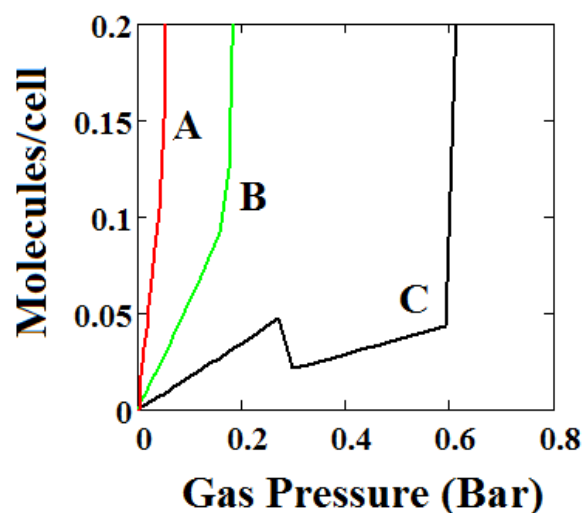


Fig. 9. Plot of the behaviour of the methane adsorption in the theory MOF for 3 pairs of differences in values of the LP and NP heats of adsorption (A= -13.00/-18.96, B = -16.6/ -13.55, C = -14.8/-13.55 kJ/mole). Curve C shows a NGA transformation at low pressure on the left. For the NGA transformation to occur the LP, NP heats of adsorption should be close in magnitude. The other parameters are $T=257$ K, $J=-1.08$ kJ/mole, $\Delta=0.025$ kJ/mole, $X=5000\text{\AA}^3$, $Y=10000\text{\AA}^3$, $N_m=40$, $scale=0$, $n_{maxlp}=21$, $n_{maxnp}=20$.

9. Conclusions

In this paper we have presented the outcomes of a basic theoretical investigation of methane adsorption in large pore MOFs with the aim of establishing the unique features of this phenomenon relevant to the question of methane storage for energy applications. We have developed a pseudo one-dimensional statistical mechanical theory of adsorption of gas in a MOF with both narrow and large pores which is solved exactly using a transfer matrix technique in the Osmotic Ensemble (OE). The theory effectively allows the distinctive features of adsorption of gas isotherms in MOFs to be described. The characteristic form of adsorption isotherms in MOFs reflect changes in structure caused by adsorption of gas and compressive stress. Of extraordinary importance for gas storage for energy applications we find two regimes of Negative adsorption of gas (NGA) where gas pressure causes the MOF to transform from the large pore to the narrow pore structure. These transformations can be induced by mechanical compression and conceivably used in an engine to discharge adsorbed gas from the MOF. The elements which govern NGA in MOFs with large pores are identified.

Although it might appear that some of our conclusions are unfavourable when it comes to using MOFs in energy storage this is not the case. For example, the negative gas adsorption phenomena which we discuss can be advantageously used in the release of gas from an MOF. There seems to be numerous possibilities around this issue.

In certain situations the NGA phenomenon may prove to be disadvantageous. However, it seems possible by use of chemical design to arrange the crystal energetics to eliminate this phenomenon, so that the narrow pore plays no effective role in the adsorption.

We have given no discussion to mixture adsorption [30] in these large pore MOFs. Yet, again there are many interesting questions and possibilities surrounding this issue.

Finally, we fully appreciate that our study, which to some extent is preliminary, raises many theoretical and experimental questions around the use of MOFs as energy storage materials.

Competing Interests: The authors have no competing interests.

Authors' Contributions: Both authors contributed equally to the development of all aspects of this study.

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51. The mathematical software used (Mathcad 15) is available from: Mathcad 15, Parametric Technology Corporation, 140 Kendrick Street, Needham, MA 02494 USA.



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